AN IMPROVED PROCESS FOR THE PREPARATION OF MONOKETALS OF 1,4-CYCLOHEXANEDIONE INCLUDING 1, 4-CYCLOHEXANEDIONE MONO–2, 2-DIMETHYL TRIMETHYLENE KETAL

# CROSS REFERENCE TO RELATED APPLICATIONS

[0001] This application claims benefit of the filing date of Indian Patent Application No. 681/MAS/2002, filed September 13, 2002, the content of which is expressly incorporated herein by reference in its entirety.

#### FIELD OF THE INVENTION

[0002] The present invention relates to an improved process for the preparation of monoketals of 1,4-cyclohexanedione, including 1, 4-cyclohexanedione mono-2, 2-dimethyl trimethylene ketal, an intermediate for a number active pharmaceutical ingredients (API) including frovatriptan.

### BACKGROUND OF THE INVENTION

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for preparation of 1, 4-cyclohexanedione mono-2, 2-dimethyl trimethylene ketal that includes continuous extraction of an aqueous solution of 1,4-cyclohexane dione containing 2,2-dimethyl -1,3-propane diol in molar excess and sulfuric acid as the catalyst to afford the 1,4 cyclohexanedione mono -2,2 -dimethyl trimethylene ketal. Nevertheless, there is still a need for an improved process suitable for a commercial scale production of 1, 4-cyclohexanedione mono-2, 2-dimethyl trimethylene ketal

and structurally related compound.

## SUMMARY OF THE INVENTION

[0005] In accordance with one aspect, the invention provides an improved process for preparation of monoketals of 1, 4-cyclohexanediones of the structure

[0006] In one embodiment, the process includes reacting 1,4-cyclohexanedione of the structure

with a diol of the structure

in a halogenated organic solvent in the presence of an acid catalyst, where X is substituted or unsubstituted ethylene or propylene. In another embodiment, the invention provides for preparing 1, 4-cyclohexanedione mono-2, 2-dimethyl trimethylene ketal that includes reacting 1,4-cyclohexanedione of the structure

with a diol of the structure

in a halogenated organic solvent in the presence of an acid catalyst. In another embodiment, the process includes

- a. reacting 1,4-cyclohexanedion and neopentyl glycol in a halogenated solvent in the presence of an acid catalyst;
- b. removing the halogenated solvent to provide a crude residue;
- c. providing said crude residue in an aliphatic or alicyclic hydrocarbon solvent to form a mixture; and
- d. filtering the mixture.

# DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

[0007] The preparation of a monoketal of 1, 4-cyclohexanedione may include a condensation reaction of 1,4-cyclohexanedione with a diol having the structure

where X is a substituted or unsubstituted ethylene or propylene. Non-limiting examples of suitable diols include ethylene glycol, propylene glycol, neopentyl glycol or 1,3-propanediol. Particularly, when the diol is neopentyl glycol, the product of the condensation is 1, 4-cyclohexanedione mono-2, 2-dimethyl trimethylene ketal. In a

particular embodiment, the invention therefore provides a process for preparation of 1, 4-cyclohexanedione mono-2, 2-dimethyl trimethylene ketal via a reaction between neopentyl glycol and 1,4-cyclohexanedione.

The reaction is carried out in a halogenated solvent in the presence of acid catalyst. For example, 1,4-cyclohexanedione and the diol may be dissolved together in the halogenated solvent before the acid catalyst is added thereto. Alternatively, the solution of each reactant may be prepared separately and later combined in a desired order. The halogenated solvent is preferably C<sub>1</sub>-C<sub>3</sub> haloalkane. Non-limiting examples of suitable C<sub>1</sub>-C<sub>3</sub> haloalkanes include chloroform, dichloromethane, dichloroethane, carbon tetrachloride, and mixtures thereof. The acid catalyst of the process can be any conventional acids, which is preferably adoptable for a commercial scale of the reaction and can be used in the halogenated solvents of the process. Non-limiting examples of suitable acid catalysts are hydrochloric acid, p-toluenesulfonic acid, sulfuric acid, fumaric acid, phthalic acid, oxalic acid and mixtures thereof. The acid catalyst may be supplied to the condensation reaction by itself or in a solvent.

[0009] The condensation reaction may be carried out at an ambient temperature or elevated temperature. The preferred temperature range for the condensation reaction is between about 25°C and about 50°C, more preferably between about 25°C and about 30°C.

[0010] The molar ratio between 1,4-cyclohexanedion and the diol to be used in the condensation reaction preferably ranges from about 1:1 to about 1:4; more preferably the range is from about 1:1 to about 1:2; and yet more preferably the molar ratio is about 1:1. However, the molar ratio may be altered, if desired. For example, the smaller amount of the diol than that of 1,4-cyclohexanedion may be used in the condensation reaction although the reaction yield may be affected thereby. In the condensation reaction of this aspect of the invention, the weight/volume ratio of 1,4-

cyclohexanedion to the halogenated organic solvent preferably ranges from about 1:1 to about 1:20, and more preferable the weight/volume ratio is about 1:8.

[0011] It is believed that the process of this aspect of the invention leads to desired intermediates having higher purities than the prior art processes. Also, the process is more suitable for commercial production of the intermediates.

Upon completion of the condensation reaction, the reaction mixture can be subjected to a conventional work-up and isolation procedures. One preferred work-up and isolation process includes washing the reaction mixture with an aqueous base solution; separating the organic layer from resulting biphasic mixture; removing the organic solvent from the separated organic layer to give a crude residue; providing the crude residue in aliphatic or alicyclic hydrocarbon solvent to form a mixture; removing solid impurities from the mixture; and isolating the monoketal product.

[0013] The washing of the condensation reaction mixture with an aqueous base can be done preferably at about 0-25°C, more preferably at about 10-20°C. The aqueous base can be water solution of any typical bases as long as it does not affect the stability of the monoketal product. Preferable examples of the base include potassium carbonate, calcium carbonate, ammonium hydroxide and mixtures thereof.

The organic solvent of the organic layer may be removed under reduced pressure but may not have to be removed completely to give essentially dry solid crude residue. A residual amount of the organic solvent left over in the crude residue may be acceptable, especially if it does not affect the followed filtration process using the aliphatic or alicyclic hydrocarbon solvent. Before removal of the organic solvent, the organic layer may be dried over drying agents such as, for example, magnesium sulfate, molecular sieves, etc.

[0015] Non-limiting examples of suitable aliphatic or alicyclic hydrocarbon solvents for work-up and isolation process include petroleum, ether, hexane, n-hexane,

cyclohexane, n-heptane, cycloheptane or mixtures thereof. The crude residue may be combined with the aliphatic or alicyclic hydrocarbon does not have to be an essentially dried solid. The removal of solid impurities from the reaction mass can be easily obtained by conventional filtration techniques. For example, the filtration can be done using filtration papers or short silica gel columns. Other conventional techniques, which are suitable for such separation of solid impurities from a solution, may also be used. The filtration techniques may be performed at a temperature preferably between about 0°C and about 25°C, more preferably between about 0°C and about 5°C. After filtration, the solvent may be optionally distilled off from the filtrate preferably under reduced pressure.

[0016] Since the monoketal product of the present invention is mostly likely to be used as a precursor of other compounds such as (+)-(R)-2,3,4,9-tetrahydro-3-(methylamino)-1H-carbazole-6-carboxamide butanedioate, frovatriptan, the isolated monoketal product may be isolated as a solution, solid or wet solid in which the solvent is not completely removed depending upon the characteristics of the use of the monoketal product.

[0017] Thus, another aspect of the present invention includes preparation of frovatriptan using the process described herein. The process for frovatriptan may require conversion of the monoketal product to a ketal of the formula:

and cyclization of the ketal with 4-carboxamidophenylhydrazine. The detailed conditions for the processes of preparing Frovatriptan are known in the art, such as the methods described in U.S. Patent No. 5,618,847, the entire content of which is herein

incorporated by reference. For example, the desired ketal may be prepared by a reaction of the monoketal with methylamine. This reaction may be effected in a suitable solvent, for example a hydrocarbon such as benzene or toluene in the presence of titanium tetrachloride or suitable molecular sieves e.g. 4 Å molecular sieves, to give the corresponding iminoketal derivative which may then be converted to an alkylamino compound by catalytic hydrogenation using, for example, palladium on carbon. Alternatively the reaction may be effected in a solvent such as an alcohol, e.g. ethanol and the mixture hydrogenated directly, using, e.g., palladium on charcoal, to give the ketal compound.

[0018] The invention is illustrated by the following examples, which are not intended to limit the effective scope of the claims.

### Example 1

1,4 cyclohexane dione (20.0 grams) and neopentyl glycol (18.6 grams) were dissolved in dichloromethane (160 ml). Then sulfuric acid (3.2 grams) was added to the reaction solution at an ambient temperature and stirred till the reaction substantially completes, accompanied by cooling the reaction mixture to 10-20°C. The resulting reaction mixture was washed with saturated aqueous sodium bicarbonate solution (80 ml) and separated the organic layer from the resulting biphasic mixture. The solvent was distilled off from organic layer till substantial completion under reduced pressure. Hexane (200 ml) was added to the resulting residual mass and followed by cooling the reaction mass to a temperature of 0-5°C to filter the byproducts. Then the solvent from the filtrate was distilled off till the substantial completion under vacuum to yield the desired 1,4 cyclohexanedione mono -2,2 - dimethyl trimethylene ketal.

(Weight: 22.9 grams)

#### Example 2

1,4 cyclohexane dione (25.0 grams) and neopentyl glycol (23.5 grams) were dissolved in chloroform (200 ml). Then sulfuric acid (4.0 grams) was added to the reaction solution at an ambient temperature and stirred till the reaction substantially completes, accompanied by cooling the reaction mixture to 10-20°C. The resulting reaction mixture was washed with saturated aqueous sodium bicarbonate solution (100 ml) and separated the organic layer from the resulting biphasic mixture. The solvent was distilled off from organic layer till substantial completion under reduced pressure.

Hexane (250 ml) was added to the resulting residual mass and followed by cooling the reaction mass to a temperature of 0-5°C to filter the by-products. Then the solvent from the filtrate was distilled off till the substantial completion under vacuum to yield the desired 1,4 cyclohexanedione mono -2,2 – dimethyl trimethylene ketal.

(Weight: 29.0 grams)

## Example 3

1,4 cyclohexane dione (25.0 grams) and neopentyl glycol (23.5 grams) were dissolved in dichloromethane (200 ml). Then sulfuric acid (4.0 grams) was added to the reaction solution at an ambient temperature and stirred till the reaction substantially completes, accompanied by cooling the reaction mixture to 10-20°C. The resulting reaction mixture was washed with saturated aqueous sodium bicarbonate solution (100 ml) and separated the organic layer from the resulting biphasic mixture. The solvent was distilled off from organic layer till substantial completion under reduced pressure. n-Heptane (250 ml) was added to the resulting residual mass and followed by cooling the reaction mass to a temperature of 0-5°C to filter the byproducts. Then the solvent from the filtrate was distilled off till the substantial completion under vacuum to yield the desired 1,4 cyclohexanedione mono -2,2 - dimethyl trimethylene ketal.

(Weight: 30.0 grams).

[0022] Unless stated to the contrary, any use of the words such as "including," "containing," "comprising," "having" and the like, means "including without limitation" and shall not be construed to limit any general statement, the specific or similar items or matters immediately following it. Except where the context indicates to the contrary, all exemplary values are intended to be fictitious, unrelated to actual entities and are used for purposes of illustration only. Most of the foregoing alternative embodiments are not mutually exclusive, but may be implemented in various combinations. As these and other variations and combinations of the features discussed above can be utilized without departing from the invention as defined by the claims, the foregoing description of the embodiments should be taken by way of illustration rather than by way of limitation of the invention as defined by the appended claims.